



A Better Approach To Energy Performance Benchmarking

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Current Industry Challenges



- High energy costs driving need for improved efficiency
- The industry is asking:
 - What is the best I can do with my existing plant?
 - How do I design energy efficiency into new expansion projects?
- Effective energy performance benchmarking & analysis required to develop sound energy saving strategies



Limitations In Typical Methods



- Typical energy benchmarking approaches have inherent limitations:
 - Not based on any fundamental or intrinsic definition of energy efficiency
 - Do not indicate your best, economic attainable level of energy performance
 - Heavily influenced by process plant utilization
 - Do not take into account the correct interrelationship between a site's actual marginal fuel and power costs



Best Energy Technology (BT)



- KBC developed a “Best Energy Technology” (BT) benchmark for refineries and petrochemical plants
 - Allowance equations for individual processes and offsites
 - Ratios actual energy consumption to allowance
 - All energy converted to fuel equivalence (MMBTU/hr)
 - Actual marginal energy economics used to convert steam and power to fuel basis
 - 100% BT is ultimate achievable level of energy efficiency
 - Grass roots refinery
 - Four year or better payback hurdle, site might economically achieve 140-150 % BT
 - Less than 100% unit BT possible with latest technology



BT Characteristics - Process



- Best Technology is based on the following Process Unit characteristics:
 - Fired heater efficiency (LHV) of 92%
 - Optimum heat integration approach temperatures (delta T_{min})
 - Site Power/Heat ratio <0.6
 - No cross-pinch configurations
 - Inter-process heat integration
 - No lost heat to cool down and reheat unit feed streams
 - Favor waste heat recovery to feed versus steam generation
 - Stripping and reboiling steam rates optimized



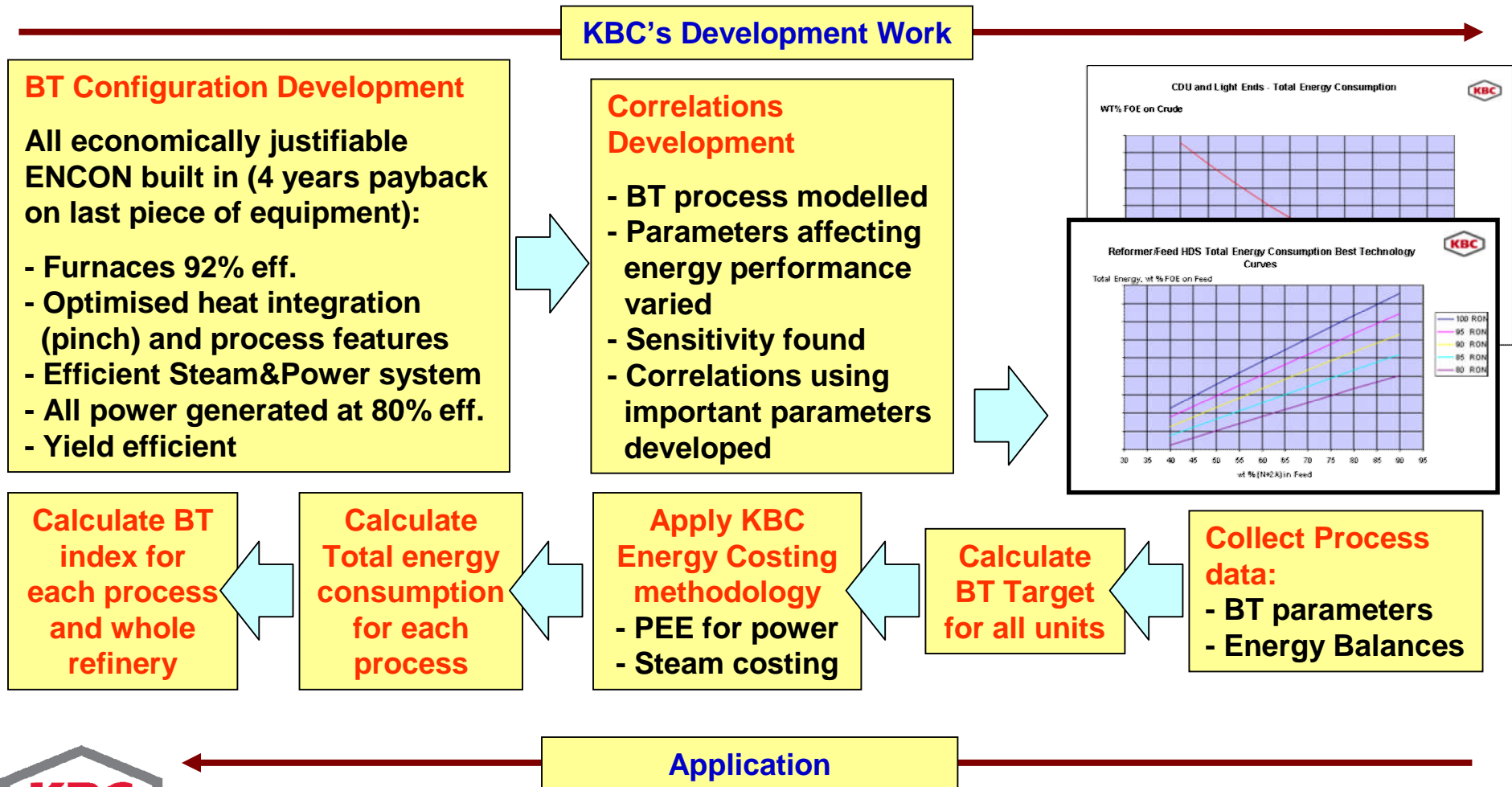
BT Characteristics - Utilities



- Best Technology is based on the following Utility System configuration:
 - 1500 psig steam system letdown to lower pressures through efficient backpressure turbines
 - Gas turbine depending on fuel and power prices
 - No steam letdowns between headers
 - No steam venting
 - Lower pressure headers supplying all process steam requirements
 - 100% plant-produced electric power
 - Optimized fuel gas composition (no excess H₂ or C₃+)



BT Benchmarking Methodology



Refinery Energy Balance



MMBTU/HR	Consumption							Supplies			
	Unit Name	Fuel	Electric	Steam	FCC Coke	Unit Total	Allow.	BT	Source	FOEB/KW	MMBTU/HR
Crude #1	575	38	79			692	414	167%	Produced Fuel	299,064	2,252
Crude #2	367	2	56			425	281	151%	Vaporizer	50,004	406
Hydrocracker	50	81	(55)			77	54	143%	Fuel Oil	27,957	227
HDS	26	18	11			55	20	271%	Purch Nat Gas	-	-
Aromatics	-	3	10			13	5	242%	Cracker Coke	186,838	1,520
SRU	11	2	(2)			11	18	63%			
Isom	-	3	24			27	9	290%	Purch Power KW	49,245	443
FCCU	-	5	88	289		382	207	185%	@37.9% PEE		
Resid Cracker	188	59	(113)	1,231		1,365	583	234%			
Alky	-	41	95			136	94	144%	Total Supplied Energy		4,848
Hydrogen Plant	178	8	(29)			158	117	135%			
Naphtha HT	175	30	45			250	62	401%			
Reformer #1	45	1	88			134	54	249%			
Reformer #2	218	5	(88)			135	140	97%			
Offsites Area	4	145	840			989	147	675%			
Facility Total	1,838	441	1,049	1,520		4,848	2,206	220%	Supply BT		
									Energy Balance	220%	100.0%



Price Equivalent Efficiency (PEE)



$$\text{PEE} = \frac{\text{Cost of 1 MMBTU of refinery marginal fuel}}{\text{Cost of 1 MMBTU of imported power}} * 100$$

- Example, if fuel at 3.50 \$/MMBTU and power at 70 \$/MWh (1 MWh = 3.414 MMBTU/hr)

$$\text{PEE} = \frac{3.50}{70 * (1/3.414)} * 100 = 17.1\%$$

- The cost of imported power is equal to the cost of generating own power at efficiency of 17.1 %.



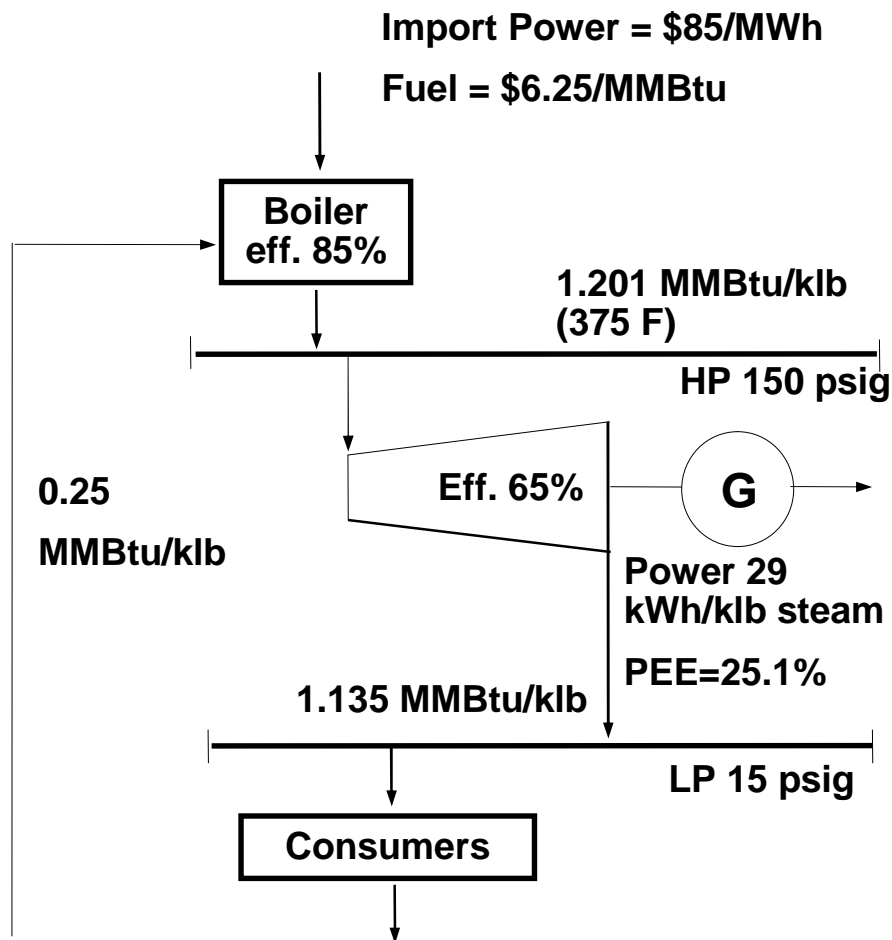
BT Steam Costing Methodology



- Costing steam on an enthalpy basis is in most cases incorrect
 - It over-estimates the cost of the LP steam - this may lead to incorrect energy strategies
- High pressure steam marginal cost is equal to the cost of producing it, i.e. cost of fuel / boiler efficiency
- Low pressure steam should be given a credit for generating power at the cost of marginal power
 - The marginal cost of LP steam is equal to the cost of HP steam less the value of the power produced from it
 - LP steam cost can be very low, even negative



Steam Costing Example



Price Equivalent Efficiency:

Cost of Fuel/Power

$$6.25 / (85/3.414) * 100 = 25.1\%$$

$$(1 \text{ MW} = 3.414 \text{ MMBtu})$$

HP steam value:

$$(1.20 - 0.25) / 0.85 = 1.12 \text{ MMBtu/klb,}$$

$$\text{Or: } 6.25 * 1.12 = 7.00 \$ / \text{klb}$$

Power credit (MW/PEE):

$$0.029 * 3.414 / .251 = 0.40 \text{ MMBtu/klb}$$

LP steam value:

$$\text{HP value} - \text{Power Credit} =$$

$$1.12 - 0.40 = 0.72 \text{ MMBtu/klb}$$

$$\text{Or: } 6.25 * 0.72 = 4.50 \$ / \text{klb}$$



Gap Analysis

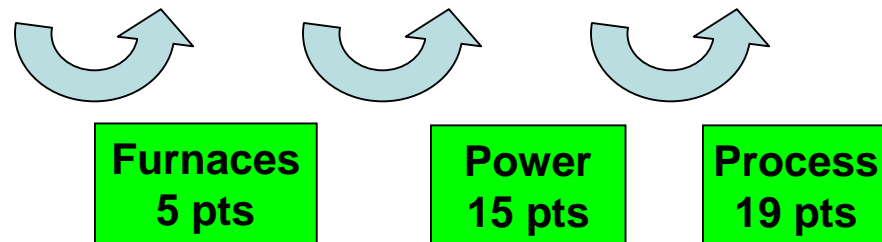


- BT Gap generally broken-down into four categories:
 - Steam Usage vs Best Practice
 - Fired Heater Efficiency
 - Shaft Work Efficiency
 - Heat Integration Effectiveness

Remainder is intrinsic inefficiencies due to design

- Analysis performed on overall basis, can be on unit by unit basis

	Base Case	Eliminate Flaring	Furnaces at 92 %	Power generation at 80%	Heat integration
Total Energy, Gcal/h	515	506	491	448	395
BT allowance, Gcal/h	287	287	287	287	287
Refinery BT index	179%	176%	171%	156%	137%



Case Study



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Questions?



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